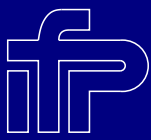


A Finite Volume Scheme for the Transport of Radionuclides in Porous Media

Presented by Guillaume Enchéry

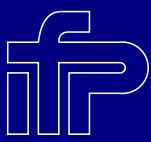
Eric Chénier, Robert Eymard, Xavier Nicolas

Université de Marne-la-Vallée



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2. Application to a simplified case
3. Numerical results
4. Concluding remarks



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Physical problems

Transport of mass and energy within porous media :

- Pollution of soils
- Degradation of concrete
- Migration of hydrocarbon components
- ...

Examples of conservation equations in porous media

N^c components, N_p phases

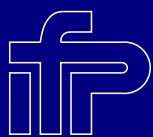
$$(A_p^c)_t + \operatorname{div} F_p^c = R_p^c$$

$$A_p^c = S_p \xi_p X_p^c$$

$$F_p^c = \xi_p X_p^c V_p - D_p^c(V_p) \cdot \nabla X_p^c$$

$$D_p^c(v) \cdot w = a_p^c w + |v| \left(b_p^c \frac{v \cdot w}{v \cdot v} v + c_p^c \left(w - \frac{v \cdot w}{v \cdot v} v \right) \right)$$

$$V_p = -K \frac{k_{rp}(S_p)}{\mu_p} (\nabla P_p - \rho_p g)$$



Mathematical questions

Existence and uniqueness of solutions

Numerical approximation

Convergence and error estimates

...

Approximation using finite volume methods

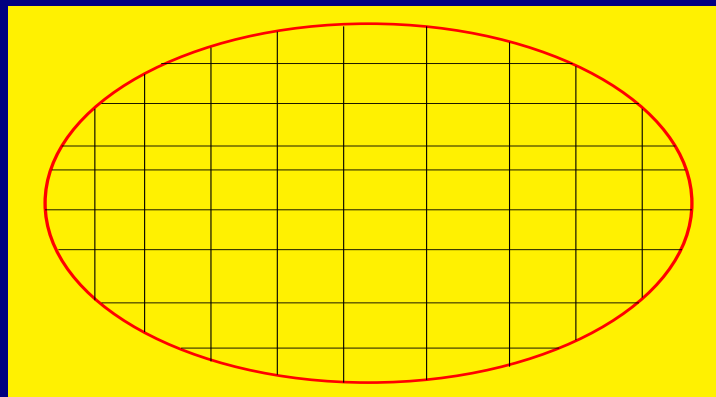
Conservation equation

$$\frac{\partial A}{\partial t} + \text{div}\mathbf{F} = R$$

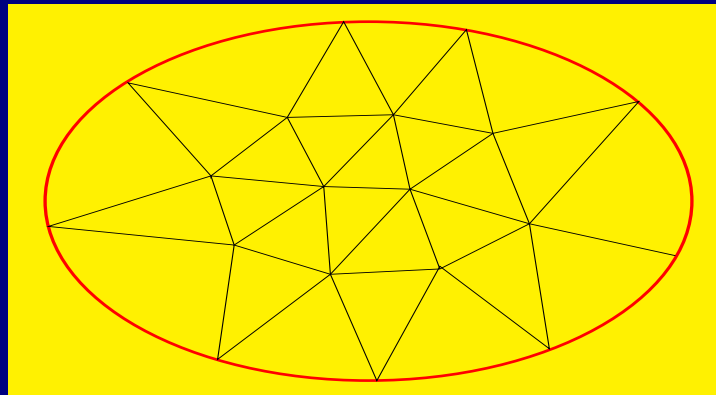
with

- A : extensive quantity
- F : flux
- R : reaction term

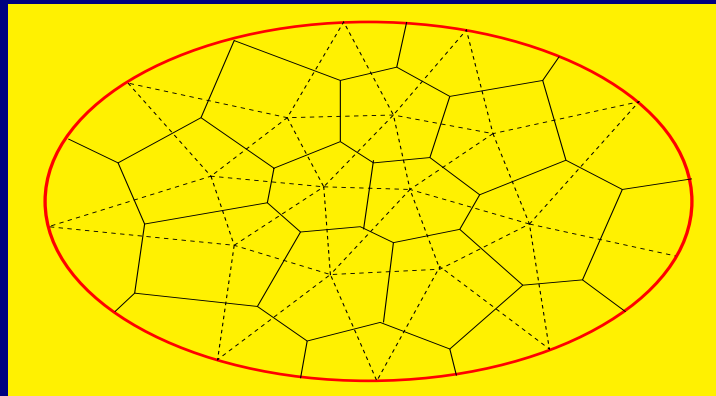
Partition of the domain



Partition of the domain



Dual mesh (Voronoi mesh)



Extensive balance in control volumes

$$m_K \frac{A_K^{(n+1)} - A_K^{(n)}}{\delta t^{(n)}} + \sum_{L \in \mathcal{N}_K} F_{K,L}^{(n,n+1)} = m_K R_K^{(n)}$$

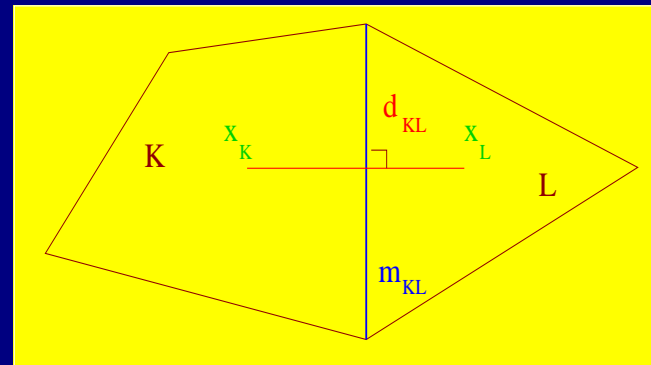
$$F_{K,L}^{(n,n+1)} \text{ approx. } \frac{1}{\delta t^{(n)}} \int_{t^{(n)}}^{t^{(n+1)}} \int_{K|L} \mathbf{F} \cdot \mathbf{n}_{K,L} ds dt$$

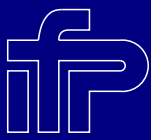
$$F_{K,L}^{(n,n+1)} = -F_{L,K}^{(n,n+1)} \Rightarrow \text{local conservation}$$

Flux approximation

Finite Difference Approximation of $\mathbf{F} = -a \nabla u$

$$F_{K,L} = -a m_{KL} \frac{u_L - u_K}{d_{KL}}$$





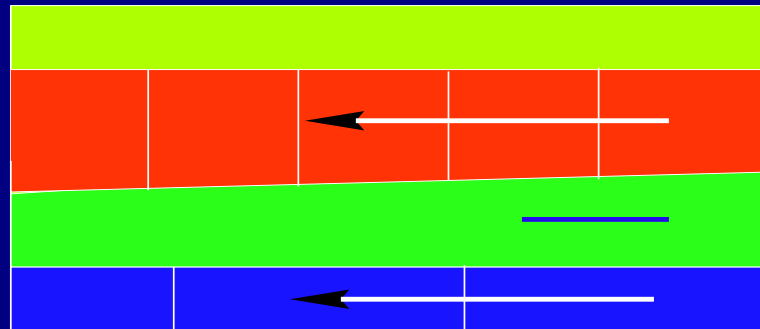
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The COUPLEX 1 case

$$\text{div} V_1 = 0 \text{ with } V_1 = -K(\nabla P_1 - \rho_1 g)$$

$$(X_1^1)_t - \text{div} \left(X_1^1 V_1 - D(V_1) \cdot \nabla X_1^1 \right) = -\Lambda X_1^1$$



Finite volume scheme on Voronoï mesh

$$H_K = P_{1K} - \rho_1 g \cdot z_K \text{ and } V_{K,L} = m_{KL} \frac{H_K - H_L}{d_{KL}}$$

$$\text{FV scheme: } \sum_{L \in N_K} V_{K,L} = 0$$

$$\frac{m_{KL}}{d_{KL}} = - \int_{\Omega} \nabla \varphi_K(x) \cdot \nabla \varphi_L(x) dx \Rightarrow \text{FV} = \text{FE}$$

approx. ∇H constant by triangle

Finite volume scheme for concentrations

$$m_K \frac{X_K^{(n+1)} - X_K^{(n)}}{\delta t} + \sum_{L \in N_K} \left[\begin{array}{c} X_{K,L}^{(m)} V_{K,L}^- \\ D_{KL} (X_L^{(m)} - X_K^{(m)}) \end{array} \right] = m_K (R_K^{(n)} - k X_K^{(n+1)})$$

with

$$D_{KL} = - \int_{\Omega} \nabla \varphi_K(x) D(\nabla H) \nabla \varphi_L(x) dx$$

$$m = n \text{ or } m = n + 1$$

Upwinding scheme

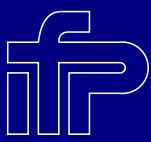
```
if  $V_{K,L} \geq 0$  then  $X_{K,L}^{(m)} = X_K^{(m)}$   
else  $X_{K,L}^{(m)} = X_L^{(m)}$ 
```

Variable Péclet number finite volume scheme

$$\begin{aligned}
 X_{K,L}^{(m)} &= \theta_{K,L} X_K^{(m)} + (1 - \theta_{K,L}) X_L^{(m)} \\
 \Rightarrow F_{K,L}^{(m)} &= \left(\theta_{K,L} X_K^{(m)} + (1 - \theta_{K,L}) X_L^{(m)} \right) V_{K,L} - \\
 &D_{KL} (X_L^{(m)} - X_K^{(m)})
 \end{aligned}$$

minimum of $|\theta_{K,L} - \frac{1}{2}|$ with $\theta_{K,L} \in [0, 1]$ and

$$\theta_{K,L} V_{K,L} + D_{KL} \geq 0, \quad (1 - \theta_{K,L}) V_{K,L} - D_{KL} \leq 0$$



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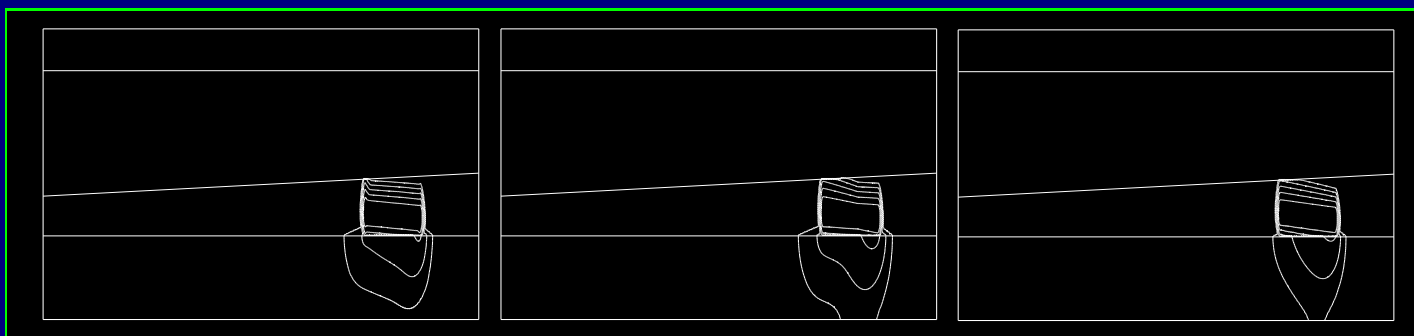
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Contour levels of iodine at 10110 years



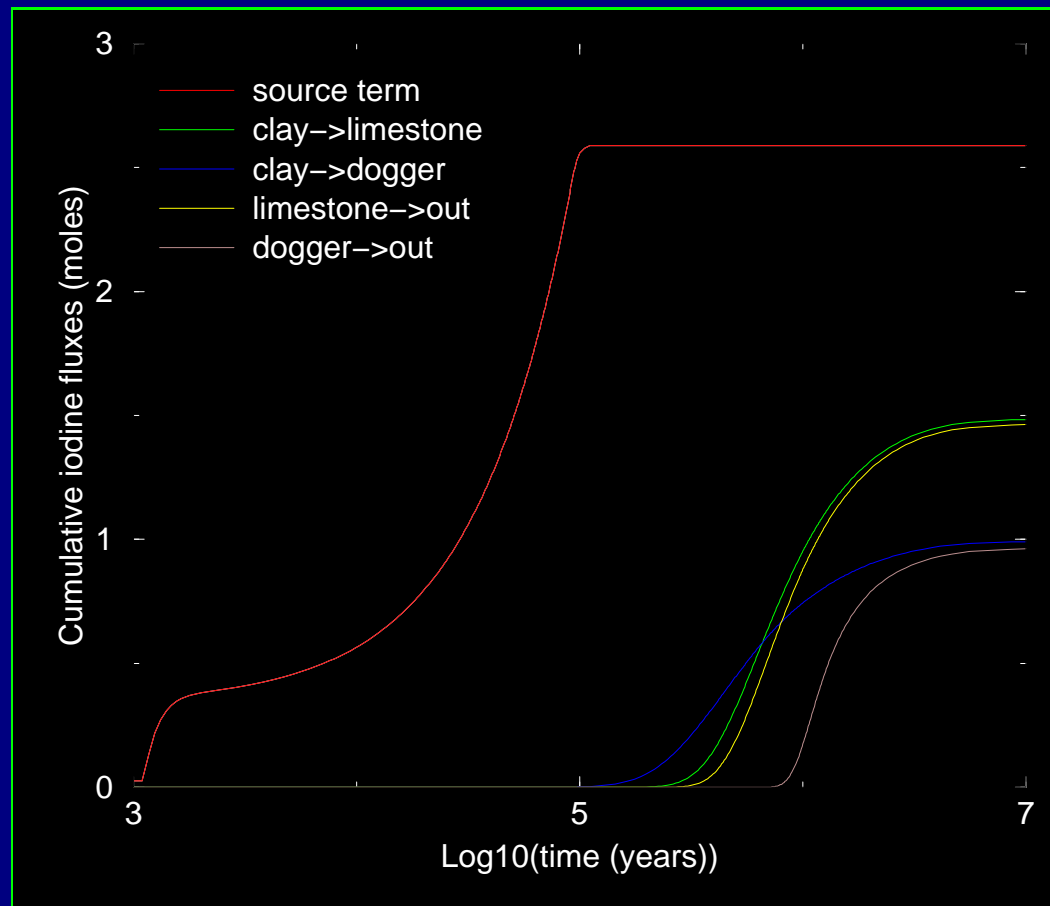
MUSCL exp. (left), up.imp. (middle), Péc.imp. (right)

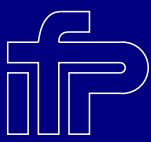
Contour levels of iodine at 50110 years



MUSCL exp. (left), up.imp. (middle), Péc.imp. (right)

Cumulative total fluxes of iodine





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Concluding remarks

1. FV simple and accurate = industrial schemes.
2. A complete engineering approach ? Handling uncertainties on
 - (a) porosity, permeability, diffusivity fields, source terms,
 - (b) boundary conditions as function of time.